



## Full length article

## A DFT study and microkinetic analysis of CO oxidation to dimethyl oxalate over Pd stripe and Pd single atom-doped Cu(111) surfaces

Bingying Han<sup>a</sup>, Lixia Ling<sup>b,c,d,\*</sup>, Maohong Fan<sup>c</sup>, Ping Liu<sup>d</sup>, Baojun Wang<sup>a,\*</sup>, Riguang Zhang<sup>a</sup><sup>a</sup> Key Laboratory of Coal Science and Technology of Ministry of Education and Shanxi Province, Taiyuan University of Technology, Taiyuan 030024, PR China<sup>b</sup> College of Chemistry and Chemical Engineering, Taiyuan University of Technology, Taiyuan 030024, PR China<sup>c</sup> Department of Chemical and Petroleum Engineering, University of Wyoming, 1000 E University Ave, Laramie, WY 82071, USA<sup>d</sup> State Key Laboratory of Coal Conversion, Institute of Coal Chemistry, Chinese Academy of Sciences, Taiyuan 030001, PR China

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## ABSTRACT

Developing low amount and high catalytic performance of Pd-based catalysts are vital for the oxidation of CO to dimethyl oxalate (DMO) in industry. In this study, Pd stripe and Pd single atom-doped Cu(111) surfaces are constructed via Pd substituting four striped Cu atoms and single Cu atom of surface layer over the Cu(111) surface, respectively, namely Pd<sub>4</sub>Cu<sub>8</sub>/Cu(111) and Pd<sub>1</sub>-Cu(111) surfaces, and two possible reaction pathways related to DMO synthesis have been studied on two surfaces employing density functional theory (DFT) calculation in combination with microkinetic analysis and subsequently compared with the cases of Pd(111) and Pd<sub>ML</sub>/Cu(111). The results show that COOCH<sub>3</sub>-COOCH<sub>3</sub> coupling pathway is superior to COOCH<sub>3</sub>-CO on Pd<sub>4</sub>Cu<sub>8</sub>/Cu(111) and Pd<sub>1</sub>-Cu(111). Moreover, the Pd<sub>1</sub>-Cu(111) surface shows highest catalytic activity for DMO generation, followed by the Pd<sub>4</sub>Cu<sub>8</sub>/Cu(111), the Pd(111) and the Pd<sub>ML</sub>/Cu(111) surface. Additionally, Pd<sub>4</sub>Cu<sub>8</sub>/Cu(111) and Pd<sub>1</sub>-Cu(111) surfaces exhibit high DMO selectivity. Thus, Pd stripe and Pd single atom-doped Cu(111) surfaces are thought to be prospective candidates to improve the catalytic performance of noble Pd and reduce its usage for CO oxidation to DMO.

## 1. Introduction

Dimethyl oxalate (DMO, (COOCH<sub>3</sub>)<sub>2</sub>), as an important chemical raw material, is widely applied in preparing pharmaceuticals, dyes, solvent, oxalic acid, and ethylene glycol (EG) [1–6], etc. The traditional synthesis method of DMO is mainly oxidative carbonylation of CH<sub>3</sub>OH, CO and O<sub>2</sub> in the liquid-phase using PdCl<sub>2</sub>-CuCl<sub>2</sub> catalysts [7]. However, this process is carried out under high pressure, and the condition is harsh. In addition, the catalyst is susceptible to deactivation due to metal poisoning or leaching, and liquid phase system is easy to corrode equipment. In recent decades, synthesis of DMO by the gas phase method was developed and increasingly prosperous. Unstable substance of methyl nitrite (CH<sub>3</sub>ONO, MN) is introduced in the gas phase method and it easily decomposes into OCH<sub>3</sub> and NO [8–10], then two OCH<sub>3</sub> radicals can be oxidatively coupled with two CO to produce DMO on Pd-based catalysts [11–13], which is described by the equation: 2CO + 2CH<sub>3</sub>ONO → (COOCH<sub>3</sub>)<sub>2</sub> + 2NO. Meanwhile, the produced NO directly desorbs [14] and rapidly reacts with O<sub>2</sub> and CH<sub>3</sub>OH to complete the regeneration of CH<sub>3</sub>ONO in the absence of any catalyst [15–18], which is shown in the equation: 2NO + 2CH<sub>3</sub>OH + 1/2O<sub>2</sub> →

2CH<sub>3</sub>ONO + H<sub>2</sub>O. The first chemical reaction can be proceeded at 0.1–0.5 Mpa and 375–415 K [19], and the second can be carried out under ambient temperature [17]. Therefore, the gas-phase method is widely adopted to produce DMO owing to moderate reaction conditions and low energy consumption.

Pd is the only metal confirmed to be excellent catalytic activity, selectivity and stability for DMO synthesis by gas-phase method and its (111) plane is demonstrated to be the main active facet for DMO formation [19]. However, the scarcity and expensive price of Pd metal as well as high Pd usage of an industrial catalyst hamper its large-scale and sustainable industrial applications [20,21]. Thus, how to reduce the usage of noble Pd meanwhile maintain high catalytic performance is the key to our research.

Pd-based bimetallic catalysts that cheaper metal substrates are doped by a trace amount of Pd atoms can be as a strategy to lower Pd usage and enhance the catalytic performance [22–31]. The Cu, as a low-cost metal, is considered to be a fine support for preparation of the Pd-doped Cu bimetallic catalyst with remarkable catalytic performance. Cai et al. [32] synthesized carbon-supported Cu@CuPd core-shell catalysts through the galvanic replacement approach and compared their

\* Corresponding authors at: No. 79 West Yingze Street, Taiyuan University of Technology, Taiyuan 030024, PR China.

E-mail addresses: [linglixia@tyut.edu.cn](mailto:linglixia@tyut.edu.cn) (L. Ling), [wangbaojun@tyut.edu.cn](mailto:wangbaojun@tyut.edu.cn) (B. Wang).<https://doi.org/10.1016/j.apsusc.2019.02.112>

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catalytic performance for ethanol oxidation with those of the most advanced Pd/C and PdCu/C catalysts, it was found that Cu@CuPd/C catalysts showed higher catalytic activity and durability. Additionally, Cu nanotube decorated by PdCu nanoparticle was prepared via a facile seed-mediated growth approach and its catalytic activity for the formic acid oxidation was about 3.4 and 1.7 times better than those of Pd/C and PdCuNPs/C catalysts, which validated the results of previous DFT prediction [33]. More recently, Pd<sub>1</sub>-Cu single-atom alloy catalysts that Cu substrates are doped by isolated, individual Pd atoms, have attracted tremendous attention owing to its extraordinary catalytic performance and maximum Pd atom utilization efficiency [34–49]. Experimentally, individual Pd atom doped in Cu(111) surface has been fabricated by chemical vapor deposition method and it exhibited more supreme catalytic activity for H<sub>2</sub> dissociation than Pd monolayer supported on Cu substrate or pure Pd [50]. An another important example of Cu-alloyed Pd single atoms nanoparticles were synthesized by galvanic replacement, where a small amount of Pd atoms were isolatedly doped onto the surface of Cu nanoparticles, and it showed more excellent catalytic activity toward phenylacetylene hydrogenation in contrast to either monometallic catalyst [51]. Besides, the Pd<sub>1</sub>-Cu single-atom alloy catalyst was fabricated through the incipient wetness coimpregnation approach and its catalytic performance toward acetylene semihydrogenation was significantly superior to that of either monometallic [52].

It is known that different amounts of Pd atoms from monolayer to single atom deposited on the Cu(111) surface have been successfully prepared by using vapor deposition method or galvanic replacement [32,50]. And, previous work showed Pd monolayer-doped the Cu(111) surface, i.e. Pd<sub>ML</sub>/Cu(111) surface, exhibited a slightly lower catalytic activity toward DMO synthesis as compared to the case on the Pd(111) surface, but interestingly, DMO synthesis mainly occurred on striped Pd atoms of surface layer on the Pd<sub>ML</sub>/Cu(111) surface [12]. Additionally, the catalytic performance of Pd single atom-doped Cu(111) surface toward DMO formation is also unclear and remains to be studied. Nowadays, theoretical calculation based on density functional theory (DFT) with microkinetic analysis has played as an important role in designing novel catalysts [53–65]. Based on this, Pd stripe and Pd single atom-doped Cu(111) surfaces, namely Pd<sub>4</sub>Cu<sub>8</sub>/Cu(111) and Pd<sub>1</sub>-Cu(111) surfaces, are constructed via Pd replacing four striped Cu atoms and single Cu atom of surface layer over the Cu(111) surface, respectively, and investigated toward DMO synthesis, which are compared with the cases of Pd<sub>ML</sub>/Cu(111), to simulate the catalytic performance of different amounts of Pd atoms doped on Cu(111) surfaces in experiment. It is anticipated that the results of this work can help rationally design low-cost and high catalytic performance Pd-based bimetallic catalysts.

Additionally, one metal doped on another metal substrate can give rise to strain effect that refers to stress compression or tension caused by substrate metal toward doped metal and ligand effect that arises from charge transfer between doped metal and substrate metal, resulting in unique catalytic performance of bimetallic catalysts [66–75]. Zhang et al. [66] investigated CO oxidation on Au-doped Pd(111), and found that appropriate amount of Au atoms could promote the reaction of CO oxidation, which was ascribed to weak strain effect and strong ligand effect. However, how the strain and ligand affect DMO generation on Pd<sub>4</sub>Cu<sub>8</sub>/Cu(111) and Pd<sub>1</sub>-Cu(111) is still unknown and remains to be elucidated.

## 2. Computational methods and models

All periodic density functional theory (DFT) calculations about CO oxidation to DMO were implemented within the VASP (Vienna Ab-initio Software Package) [76–78]. Projector-augmented wave (PAW) pseudopotentials was adopted to depict electron-ion interaction [79–81]. The exchange-correlation functional has been depicted by Perdew-Burke-Ernzerhof (PBE) [82] within the generalized gradient

approximation (GGA). A (3 × 2 × 1) Monk-horst-Pack k-point mesh was employed in the Brillouin zone sampling. The plane wave being 400 eV cutoff energy was set to expand the electronic wave functions. Self-consistent iteration during the geometry optimizations were converged until forces and electronic energy on the unconstraint atoms were less than 0.03 eV·Å<sup>-1</sup> force difference and 1 × 10<sup>-5</sup> eV energy change. The transition states (TSs) of each elementary reaction about DMO formation were searched to obtain the favorable reaction path. Firstly, the image which was close to the structure of transition state was located through the climbing-image nudged elastic band (CI-NEB) method [83,84]. Then, it was relaxed again via using the dimer approach [85,86] until the atomic force was smaller than 0.05 eV/Å and finally verified by frequency analysis. All electronic energies are corrected by the zero point energy (ZPE):  $ZPE = \sum_{i=1}^{3N} \frac{h\nu_i}{2}$  (1), where h and ν<sub>i</sub>

refer to the Planck constant and the calculated real frequency, respectively. The reaction energy (ΔE) and activation energy (E<sub>a</sub>) can be obtained via the following formulas:  $\Delta E = E_{FS} - E_{IS}$  (2) and  $E_a = E_{TS} - E_{IS}$  (3), where E<sub>FS</sub> stands for the energy of final state, E<sub>IS</sub> refers to that of initial state, as well as E<sub>TS</sub> represents that of transition state. The harmonic transition state theory (TST) [87] has been employed into calculating the rate constant for each reaction step:

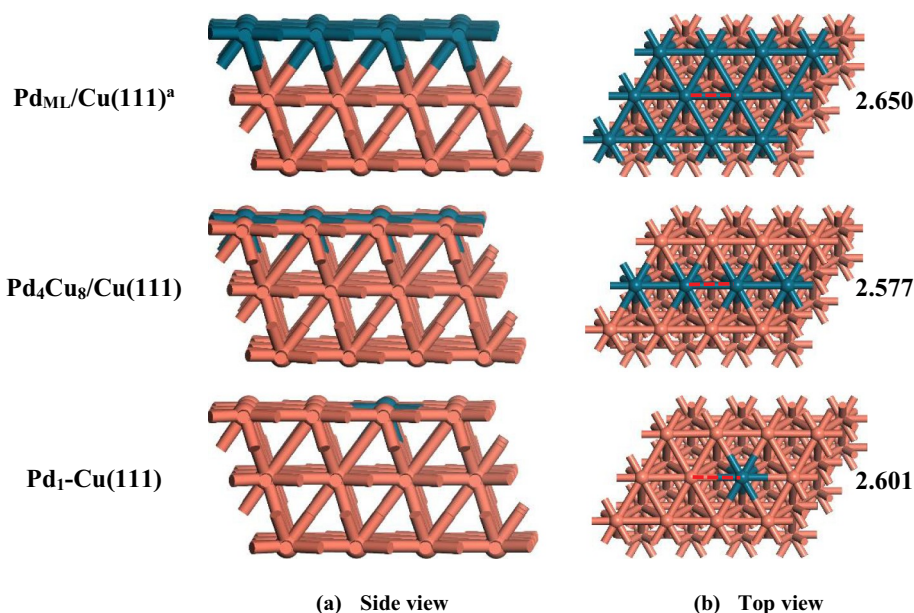
$$k = \frac{k_B T}{h} \frac{\prod_{i=1}^{3N} \left[ 1 - \exp\left(-\frac{h\nu_i^{IS}}{k_B T}\right) \right]}{\prod_{i=1}^{3N-1} \left[ 1 - \exp\left(-\frac{h\nu_i^{TS}}{k_B T}\right) \right]} \exp\left(-\frac{E_a}{RT}\right) \quad (4),$$

where k<sub>B</sub> and T stand for Boltzmann constant and the temperature. In addition, ν<sub>i</sub><sup>IS</sup> and ν<sub>i</sub><sup>TS</sup> stand for the real vibrational frequencies in the initial and transition states, respectively.

In this work, the lattice parameters (3.955 and 3.623 Å) of optimized bulk Pd and Cu by DFT well agree with the experimentally observed values (3.900 [88] and 3.615 Å [89]). The pure Cu(111) surface is firstly built by using a p(3 × 4) unit cell containing three-metal layers, then four striped Cu atoms and single Cu atom of surface layer are replacing with Pd atoms to represent Pd stripe and Pd single atom-doped Cu(111) surfaces, i.e. Pd<sub>4</sub>Cu<sub>8</sub>/Cu(111) and Pd<sub>1</sub>-Cu(111), ultimately their supercells are optimized. This method was adopted to build Pd<sub>ML</sub>/M(111) surfaces (M = Co, Ni, Cu, Al) with three-atomic-layer [11,12]. Meanwhile, the vacuum region of 10 Å is adopted in order to avoid the influence of the periodically repeated slabs. During the calculations, the upper two layers and the adsorbed species are permitted to relax while bottom one layer remains frozen. (See Fig. 1.)

To confirm the sufficiency of the selected cutoff energy (400 eV) and k-point mesh (3 × 2 × 1), we firstly compare the adsorption energies of CO on the Pd top site over Pd<sub>4</sub>Cu<sub>8</sub>/Cu(111) and Pd<sub>1</sub>-Cu(111) surfaces at the cutoff energy of 400 eV with those at the cutoff energy of 450 and 500 eV, respectively. The results show that the corresponding adsorption energies are -87.0, -84.8 and -85.7 kJ/mol on the Pd<sub>4</sub>Cu<sub>8</sub>/Cu(111) surface, -101.2, -99.0 and -99.8 kJ/mol on the Pd<sub>1</sub>-Cu(111) surface, implying that the adsorption energy does not change very much when the cutoff energy is beyond 400 eV. Then, the adsorption energy of CO with the k-point mesh (3 × 2 × 1) is compared with those at the k-point mesh of 4 × 3 × 1 and 5 × 4 × 1, respectively, indicating that the corresponding adsorption energies are -87.0, -84.5 and -87.9 kJ/mol on the Pd<sub>4</sub>Cu<sub>8</sub>/Cu(111) surface, -101.2, -98.4 and -102.1 kJ/mol on the Pd<sub>1</sub>-Cu(111) surface, which implies that there has little influence on the same catalysts when k-point mesh increases (see Table 1). Therefore, considering the calculation efficiency, the selected cutoff energy (400 eV) and k-point mesh (3 × 2 × 1) are thought to be enough and suitable for our calculated systems.

Additionally, to demonstrate the selected p(3 × 4) supercell and three-layer model are sufficient for our calculated system, the adsorption energy of CO at the Pd top site on p(3 × 4) supercell model is firstly compared with those on p(4 × 4) and p(4 × 5) supercell, respectively, which are -87.0, -84.6 and -88.4 kJ/mol on the Pd<sub>4</sub>Cu<sub>8</sub>/Cu(111) surface, -101.2, -98.7 and -100.6 kJ/mol on the Pd<sub>1</sub>-Cu(111) surface, implying that the adsorption energy does not change



**Fig. 1.** The configurations of  $\text{Pd}_4\text{Cu}_8/\text{Cu}(111)$  and  $\text{Pd}_1\text{-Cu}(111)$  surfaces; (a, b) side and top view. Dark cyan and orange balls stand for Pd and Cu, respectively. <sup>a</sup> The study in Ref. [12].

**Table 1**

Test results about the effect of cut-off energy and k-point mesh on the adsorption energy (kJ/mol) of CO at the Pd top site over  $\text{Pd}_4\text{Cu}_8/\text{Cu}(111)$  and  $\text{Pd}_1\text{-Cu}(111)$  surfaces.

	Cut-off energy			K-point mesh		
	400 eV	450 eV	500 eV	$3 \times 2 \times 1$	$4 \times 3 \times 1$	$5 \times 4 \times 1$
$\text{Pd}_4\text{Cu}_8/\text{Cu}(111)$	-87.0	-84.8	-85.7	-87.0	-84.5	-87.9
$\text{Pd}_1\text{-Cu}(111)$	-101.2	-99.0	-99.8	-101.2	-98.4	-102.1

very much on the same catalysts with three different supercell sizes. Then, we compare the adsorption energy of CO on three-layer model with those on four-layer and five-layer models, respectively, indicating that the corresponding adsorption energy are -87.0, -87.9 and -85.0 kJ/mol on the  $\text{Pd}_4\text{Cu}_8/\text{Cu}(111)$  surface, -101.2, -101.8 and -100.0 kJ/mol on the  $\text{Pd}_1\text{-Cu}(111)$  surface, which implies that there has little influence when the layer of model increases. Thus, taking account of the calculation efficiency, the selected  $p(3 \times 4)$  supercell and three-layer model are also considered to be sufficient for the calculated systems.

And, we consider the influence of dipole correction on the binding energy between Pd stripe or Pd single atom with Cu(111) surface as well as the elementary reaction process. The results indicate that the binding energies with dipole correction are -1460.0 and -604.0 kJ/mol for  $\text{Pd}_4\text{Cu}_8/\text{Cu}(111)$  and  $\text{Pd}_1\text{-Cu}(111)$ , respectively, and very close to the values of -1458.6 and -603.9 kJ/mol without dipole correction, where the binding energy is obtained by the energy of model subtracting the sum of doped Pd atom energy and defective Cu(111) energy according to previous work [90]. Meanwhile, the energy barrier and reaction energy of the first elementary step ( $\text{CO} + \text{OCH}_3 \rightarrow \text{COOCH}_3$ ) are 25.4 and -40.6 (25.8 and -40.4) kJ/mol on  $\text{Pd}_4\text{Cu}_8/\text{Cu}$

(111), 55.4 and 24.0 (55.3 and 23.3) kJ/mol on  $\text{Pd}_1\text{-Cu}(111)$ , which are very close to the values obtained without dipole correction (see the values in parentheses). That all show that little difference exists when the dipole correction is added into system. Therefore, dipole correction is neglected in this study. The previous study also adopted the same treatment method owing to little influence of the dipole correction [91,92].

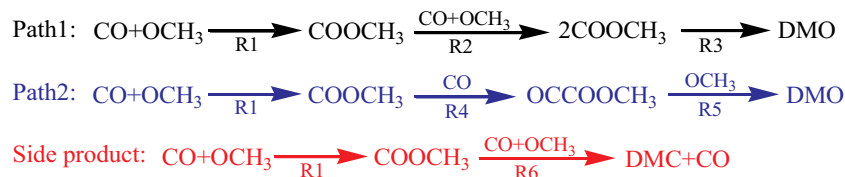
### 3. Results and discussion

#### 3.1. Catalytic activities of $\text{Pd}_4\text{Cu}_8/\text{Cu}(111)$ and $\text{Pd}_1\text{-Cu}(111)$ surfaces toward DMO formation

As is well known that  $\text{CH}_3\text{ONO}$  molecular is very easily dissociated to  $\text{OCH}_3$  radical because of the weak O-NO bond energy [8–10], therefore it is  $\text{OCH}_3$  radical that launches DMO generation. In light of different C–C coupling patterns, there exists three possible pathways for DMO formation, i.e.  $\text{COOCH}_3\text{-COOCH}_3$  coupling (Path1),  $\text{CO-COOCH}_3$  coupling (Path2) and  $\text{CO-CO}$  coupling (Path3). Among them, OCCO intermediate in Path3 is extremely unstable and easily dissociated into two CO on surfaces of  $\text{Pd}_4\text{Cu}_8/\text{Cu}(111)$  and  $\text{Pd}_1\text{-Cu}(111)$ , therefore only Path1 and Path2 will be discussed in the following sections, as shown in Scheme 1. The activation energy and reaction energy of each elementary step,  $E_a$  and  $\Delta E$ , which involved in DMO synthesis on surfaces of  $\text{Pd}_4\text{Cu}_8/\text{Cu}(111)$  and  $\text{Pd}_1\text{-Cu}(111)$ , have been presented in Table 2.

##### 3.1.1. Catalytic activity for DMO generation on the surface of $\text{Pd}_4\text{Cu}_8/\text{Cu}(111)$

The surface layer striped Pd atoms of Pd(111) and  $\text{Pd}_{\text{ML}}/\text{Cu}(111)$  have been found to be main active sites for DMO formation [12], therefore we mainly focus on investigating DMO synthesis over the Pd



**Scheme 1.** Proposed routes [13] for DMO generation via CO oxidative coupling.

**Table 2**The energy barrier and reaction heat for each elementary step ( $E_a$  and  $\Delta E$ , kJ/mol) together with the rate constant ( $k$ ,  $s^{-1}$ ) at the temperature of 395 K.

Surface	Elementary reactions	Transition state	$E_a$	$\Delta E$	$k$	
Pd <sub>4</sub> Cu <sub>8</sub> /Cu(111)	R1	CO + OCH <sub>3</sub> → COOCH <sub>3</sub>	TS1	25.8	-40.4	1.01 × 10 <sup>9</sup>
	R2	COOCH <sub>3</sub> + CO + OCH <sub>3</sub> → 2COOCH <sub>3</sub>	TS2	88.3	52.0	9.95 × 10 <sup>0</sup>
	R3	2COOCH <sub>3</sub> → (COOCH <sub>3</sub> ) <sub>2</sub>	TS3	108.8	-30.6	2.70 × 10 <sup>-2</sup>
	R4	COOCH <sub>3</sub> + CO → OCCOOCH <sub>3</sub>	TS4	139.3	74.4	3.64 × 10 <sup>-6</sup>
	R5	OCCOOCH <sub>3</sub> + OCH <sub>3</sub> → (COOCH <sub>3</sub> ) <sub>2</sub>	TS5	34.1	-74.5	3.48 × 10 <sup>7</sup>
	R6	COOCH <sub>3</sub> + CO + OCH <sub>3</sub> → DMC + CO	TS6	192.6	-52.7	4.79 × 10 <sup>-13</sup>
Pd <sub>1</sub> -Cu(111)	R1	CO + OCH <sub>3</sub> → COOCH <sub>3</sub>	TS1	55.3	23.3	1.75 × 10 <sup>5</sup>
	R2	COOCH <sub>3</sub> + CO + OCH <sub>3</sub> → 2COOCH <sub>3</sub>	TS2	65.5	34.0	4.91 × 10 <sup>3</sup>
	R3	2COOCH <sub>3</sub> → (COOCH <sub>3</sub> ) <sub>2</sub>	TS3	91.6	-26.4	4.42 × 10 <sup>1</sup>
	R4	COOCH <sub>3</sub> + CO → OCCOOCH <sub>3</sub>	TS4	130.0	55.0	5.31 × 10 <sup>-4</sup>
	R5	OCCOOCH <sub>3</sub> + OCH <sub>3</sub> → (COOCH <sub>3</sub> ) <sub>2</sub>	TS5	58.8	-41.0	2.38 × 10 <sup>4</sup>
	R6	COOCH <sub>3</sub> + CO + OCH <sub>3</sub> → DMC + CO	TS6	107.5	-27.7	5.45 × 10 <sup>-3</sup>
Pd <sub>ML</sub> /Cu(111) <sup>a</sup>	R1	CO + OCH <sub>3</sub> → COOCH <sub>3</sub>	TS1	15.6	-87.5	6.07 × 10 <sup>9</sup>
	R2	COOCH <sub>3</sub> + CO + OCH <sub>3</sub> → 2COOCH <sub>3</sub>	TS2	45.6	-25.7	1.51 × 10 <sup>6</sup>
	R3	2COOCH <sub>3</sub> → (COOCH <sub>3</sub> ) <sub>2</sub>	TS3	132.2	-34.1	6.98 × 10 <sup>-6</sup>
	R4	COOCH <sub>3</sub> + CO → OCCOOCH <sub>3</sub>	TS4	151.5	84.3	1.01 × 10 <sup>-7</sup>
	R5	OCCOOCH <sub>3</sub> + OCH <sub>3</sub> → (COOCH <sub>3</sub> ) <sub>2</sub>	TS5	166.1	-130.2	2.00 × 10 <sup>-8</sup>
	R6	COOCH <sub>3</sub> + CO + OCH <sub>3</sub> → DMC + CO	TS6	194.8	-172.4	5.10 × 10 <sup>-13</sup>
Pd(111) <sup>a</sup>	R1	CO + OCH <sub>3</sub> → COOCH <sub>3</sub>	TS1	38.1	-25.6	3.97 × 10 <sup>6</sup>
	R2	COOCH <sub>3</sub> + CO + OCH <sub>3</sub> → 2COOCH <sub>3</sub>	TS2	52.5	-17.5	5.87 × 10 <sup>4</sup>
	R3	2COOCH <sub>3</sub> → (COOCH <sub>3</sub> ) <sub>2</sub>	TS3	120.6	53.6	3.35 × 10 <sup>-5</sup>
	R4	COOCH <sub>3</sub> + CO → OCCOOCH <sub>3</sub>	TS4	160.1	117.0	2.12 × 10 <sup>-9</sup>
	R5	OCCOOCH <sub>3</sub> + OCH <sub>3</sub> → (COOCH <sub>3</sub> ) <sub>2</sub>	TS5	31.2	-43.2	6.81 × 10 <sup>8</sup>
	R6	COOCH <sub>3</sub> + CO + OCH <sub>3</sub> → DMC + CO	TS6	153.5	-110.8	1.79 × 10 <sup>-8</sup>

<sup>a</sup> The study in Ref. [12].

stripe of the Pd<sub>4</sub>Cu<sub>8</sub>/Cu(111) surface. Firstly, Path1 is initiated by co-adsorption of CO and OCH<sub>3</sub>, where OCH<sub>3</sub> and CO are adsorbed at Pd–Pd bridge and Pd top sites with co-adsorption energy being -224.1 kJ/mol, which is revealed in Fig. 2. Subsequently, OCH<sub>3</sub> oxidizes CO to generate a highly stable intermediate of COOCH<sub>3</sub> via TS1 with the energy barrier, reaction energy and rate constant being 25.8, -40.4 kJ/mol and 1.01 × 10<sup>9</sup> s<sup>-1</sup>, where C1...O2 distance decreases to 2.172 from 4.258 Å (All described rate constants are obtained at 395 K, as presented in Table 2. And the rate constants at other temperatures are shown in Table 3). The formed COOCH<sub>3</sub> occupies the Pd top site, as well as the other CO and OCH<sub>3</sub> bind to the Pd–Pd bridge and Pd-Cu-Cu hcp sites, respectively. Then the adsorbed OCH<sub>3</sub> and CO are activated via TS2 to generate the second COOCH<sub>3</sub> intermediate, thereby leading to COOCH<sub>3</sub>-COOCH<sub>3</sub> formation, which is endergonic (52.0 kJ/mol) together with the activation energy being 88.3 kJ/mol. The C3...O4 distance in TS2 configuration is reduced to 1.997 from 3.411 Å. Finally, DMO can be formed by the COOCH<sub>3</sub>-COOCH<sub>3</sub> intermediate self-coupling, which is exergonic (30.6 kJ/mol) with the activation energy and rate constant being 108.8 kJ/mol and 2.70 × 10<sup>-2</sup> s<sup>-1</sup>. The step is considered as the speed-controlling step in Path1, of which the activation barrier is lower to those (120.6 and 132.2 kJ/mol) while the rate constant is far bigger than those over Pd(111) and Pd<sub>ML</sub>/Cu(111) (3.35 × 10<sup>-5</sup> and 6.98 × 10<sup>-6</sup> s<sup>-1</sup>) [12]. Thus, it can be concluded that catalytic activity of Path1 on Pd<sub>4</sub>Cu<sub>8</sub>/Cu(111) is more than those on Pd(111) and Pd<sub>ML</sub>/Cu(111).

In Path2, the formed COOCH<sub>3</sub> of first step is further activated to attack CO which locates at the Pd–Pd bridge site, leading to OCCOOCH<sub>3</sub> generation through TS4 with the activation energy, reaction heat and rate constant being 139.3, 74.4 kJ/mol and 3.64 × 10<sup>-6</sup> s<sup>-1</sup>. At last, OCH<sub>3</sub> occupies on the Pd-Cu-Cu hcp site and attacks OCCOOCH<sub>3</sub> to generate DMO via TS5 with the rate constant, activation energy and reaction heat being 3.48 × 10<sup>7</sup> s<sup>-1</sup>, 34.1 and -74.5 kJ/mol. It is found that the second step, COOCH<sub>3</sub> + CO → OCCOOCH<sub>3</sub>, is the rate-controlling step of Path 2, of which activation barrier is relatively higher in comparison with that of Path1 (139.3 versus 108.8 kJ/mol). Accordingly, Path1 is considered to be the optimal reaction path on the surface of Pd<sub>4</sub>Cu<sub>8</sub>/Cu(111), which determines the catalytic activity of DMO formation.

### 3.1.2. Catalytic activity of the Pd<sub>1</sub>-Cu(111) surface for DMO generation

On basis of the research over Pd<sub>4</sub>Cu<sub>8</sub>/Cu(111), to further reduce the amount of precious metal Pd, we study CO oxidation to DMO over the Pd<sub>1</sub>-Cu(111). CO + OCH<sub>3</sub> → COOCH<sub>3</sub> is the first step of Path1, as depicted in Fig. 3, where OCH<sub>3</sub> and CO are bind to Cu–Cu and Pd–Cu bridge sites, afterwards COOCH<sub>3</sub> intermediate is generated through OCH<sub>3</sub> oxidizing CO via TS1 with the endothermic energy and activation energy being 23.3 and 55.3 kJ/mol. Additionally, the C1...O2 distance is shortened to 1.822 in TS1 from 3.553 Å. The other COOCH<sub>3</sub> can be formed through TS2, resulting in the COOCH<sub>3</sub>-COOCH<sub>3</sub> intermediate formation, which is endothermic by 34.0 kJ/mol together with a barrier energy being 65.5 kJ/mol. Lastly, the COOCH<sub>3</sub>-COOCH<sub>3</sub> intermediate self-couples to DMO via TS3, and the barrier energy of 91.6 kJ/mol, reaction energy being -26.4 kJ/mol and rate constant of 4.42 × 10<sup>1</sup> s<sup>-1</sup> are needed in this step.

In Path2, the generated COOCH<sub>3</sub> can react with CO to produce OCCOOCH<sub>3</sub> by TS4 with C1...C3 distance being 2.010 Å, and the activation barrier, reaction energy and rate constant are 130.0, 55.0 kJ/mol and 5.31 × 10<sup>-4</sup> s<sup>-1</sup>. Then, OCH<sub>3</sub> and OCCOOCH<sub>3</sub> are activated to generate DMO through TS5 with the reaction energy being -41.0 kJ/mol, activation barrier being 58.8 kJ/mol and rate constant of 2.38 × 10<sup>4</sup> s<sup>-1</sup>. As described above, R3 and R4 are the rate-controlling steps of Path1 and Path2 over the Pd<sub>1</sub>-Cu(111) with the barriers being 91.6 and 130.0 kJ/mol, respectively, implying the favorable pathway is Path1. In addition, comparing the barriers (132.2 [12], 108.8 and 91.6 kJ/mol) of the rate-controlling steps of the optimal path on surfaces of Pd<sub>ML</sub>/Cu(111) [12], Pd<sub>4</sub>Cu<sub>8</sub>/Cu(111) and Pd<sub>1</sub>-Cu(111), it is drawn that Pd<sub>1</sub>-Cu(111) is better than Pd<sub>ML</sub>/Cu(111) and Pd<sub>4</sub>Cu<sub>8</sub>/Cu(111) in terms of catalytic activity.

### 3.2. Comparison of DMO and DMC synthesis on Pd<sub>4</sub>Cu<sub>8</sub>/Cu(111) and Pd<sub>1</sub>-Cu(111) surfaces

In addition to investigating the generation of the main product DMO, we also consider side-product dimethyl carbonate (CH<sub>3</sub>OCOOCH<sub>3</sub>, DMC) synthesis. DMC can be formed by the COOCH<sub>3</sub> reacting with OCH<sub>3</sub> on the basis of co-adsorption of COOCH<sub>3</sub> + CO + OCH<sub>3</sub>, where the impact of CO on DMC formation is considered owing to excessive CO in the practical reaction [13]. On



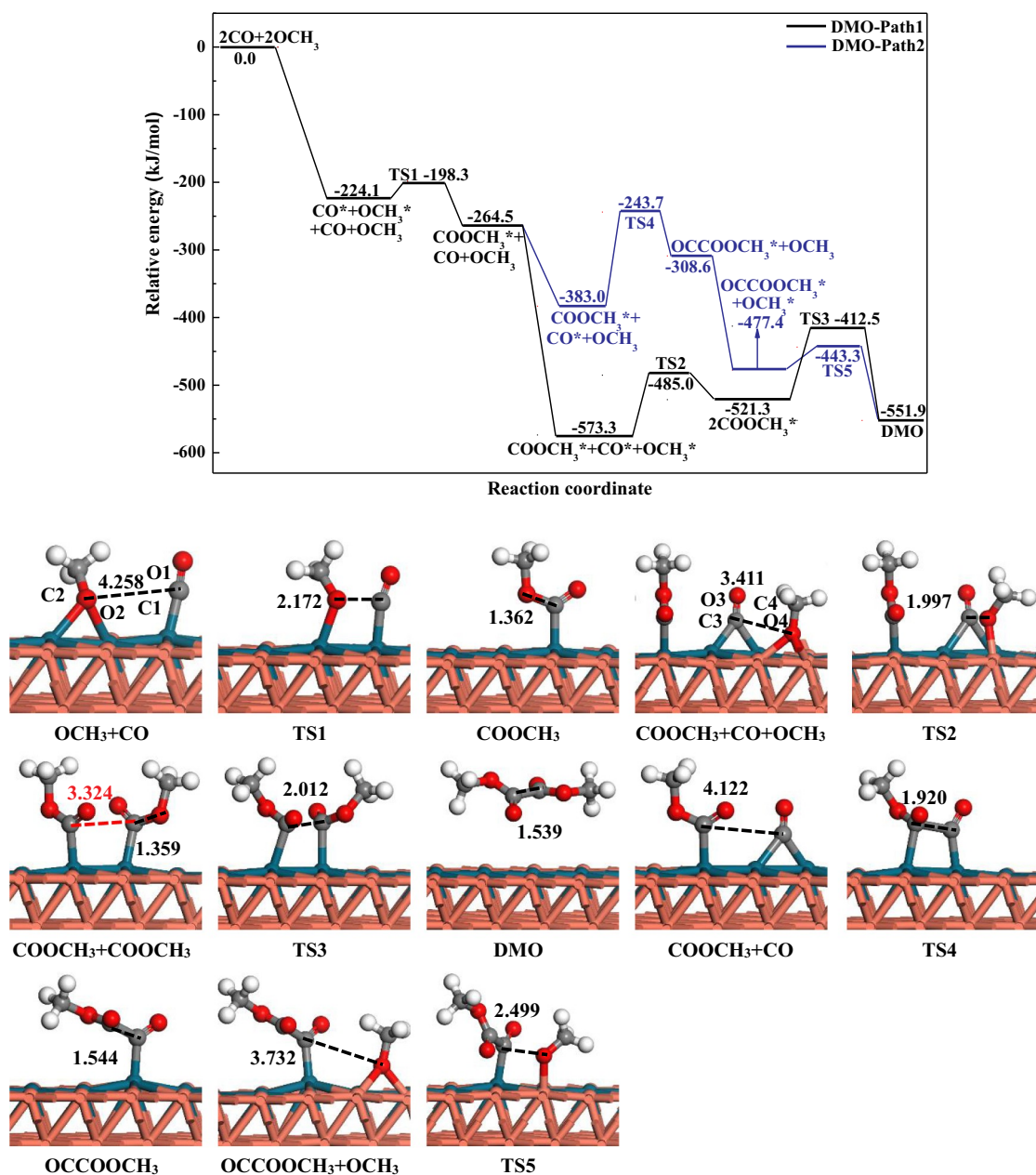


Fig. 2. Reaction energy profile of CO oxidation to DMO and relevant configurations (initial, transition and final states) over the Pd<sub>4</sub>Cu<sub>8</sub>/Cu(111).

Table 3

The rate constant ( $k$ , s<sup>-1</sup>) of each elementary step.

		375 K	385 K	395 K	405 K	415 K
Pd <sub>4</sub> Cu <sub>8</sub> /Cu(111)	$k_1$	$6.59 \times 10^8$	$8.19 \times 10^8$	$1.01 \times 10^9$	$1.23 \times 10^9$	$1.48 \times 10^9$
	$k_2$	$2.31 \times 10^0$	$4.89 \times 10^0$	$9.95 \times 10^0$	$1.96 \times 10^1$	$3.72 \times 10^1$
	$k_3$	$4.51 \times 10^{-3}$	$1.13 \times 10^{-2}$	$2.70 \times 10^{-2}$	$6.19 \times 10^{-2}$	$1.36 \times 10^{-1}$
	$k_4$	$3.69 \times 10^{-7}$	$1.19 \times 10^{-6}$	$3.64 \times 10^{-6}$	$1.05 \times 10^{-5}$	$2.88 \times 10^{-5}$
	$k_5$	$2.00 \times 10^7$	$2.66 \times 10^7$	$3.48 \times 10^7$	$4.49 \times 10^7$	$5.73 \times 10^7$
	$k_6$	$1.98 \times 10^{-14}$	$1.02 \times 10^{-13}$	$4.79 \times 10^{-13}$	$2.10 \times 10^{-12}$	$8.54 \times 10^{-12}$
Pd <sub>1</sub> -Cu(111)	$k_1$	$7.05 \times 10^4$	$1.12 \times 10^5$	$1.75 \times 10^5$	$2.66 \times 10^5$	$3.97 \times 10^5$
	$k_2$	$1.68 \times 10^3$	$2.91 \times 10^3$	$4.91 \times 10^3$	$8.07 \times 10^3$	$1.29 \times 10^4$
	$k_3$	$9.64 \times 10^0$	$2.11 \times 10^1$	$4.42 \times 10^1$	$8.95 \times 10^1$	$1.75 \times 10^2$
	$k_4$	$6.21 \times 10^{-5}$	$1.87 \times 10^{-4}$	$5.31 \times 10^{-4}$	$1.43 \times 10^{-3}$	$3.69 \times 10^{-3}$
	$k_5$	$9.00 \times 10^3$	$1.48 \times 10^4$	$2.38 \times 10^4$	$3.72 \times 10^4$	$5.71 \times 10^4$
	$k_6$	$9.57 \times 10^{-4}$	$2.34 \times 10^{-3}$	$5.45 \times 10^{-3}$	$1.22 \times 10^{-2}$	$2.62 \times 10^{-2}$

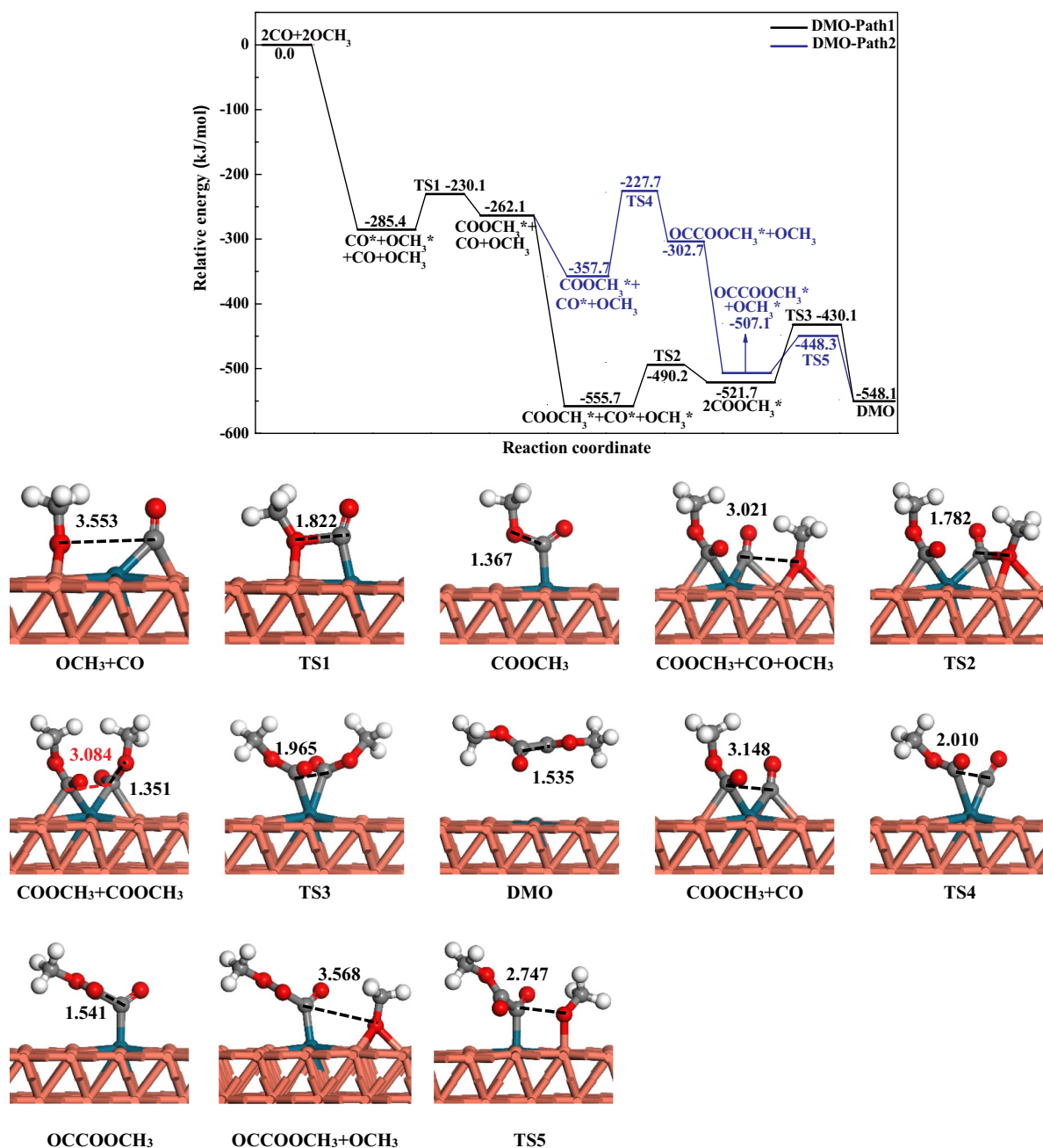


Fig. 3. Reaction energy profile of CO oxidation to DMO and relevant structures (initial, transition and final states) over the Pd<sub>1</sub>-Cu(111).

Pd<sub>4</sub>Cu<sub>8</sub>/Cu(111), it can be drawn that DMC is not favorable to be formed by comparing the energy barriers (192.6 versus 108.8) of rate-determining step in favorable path of produced DMO and DMC, which is depicted in Fig. 4. Similarly, the activation barrier (107.5 kJ/mol) of DMC generation is more than that (91.6 kJ/mol) of 2COOCH<sub>3</sub> → DMO in favorable route on the Pd<sub>1</sub>-Cu(111) surface, showing that DMO formation is significantly superior to DMC generation, which is shown in Fig. 5. Therefore, the main product DMO is more easier to be generated than the side-product (DMC) over Pd<sub>4</sub>Cu<sub>8</sub>/Cu(111) and Pd<sub>1</sub>-Cu(111).

### 3.3. Microkinetic analysis

On the basis of obtained activation energy of each elementary step, we can know that the optimal route for DMO formation is Path1 (COOCH<sub>3</sub>-COOCH<sub>3</sub> coupling) and the rate-controlling step is two COOCH<sub>3</sub> intermediates coupling to DMO. According to activation

energy for the speed-controlling step of optimal path for DMO generation, we can know that the catalytic activity is highest on the Pd<sub>1</sub>-Cu(111) surface, and Pd<sub>4</sub>Cu<sub>8</sub>/Cu(111) is higher than Pd(111), as well as Pd<sub>MI</sub>/Cu(111) exhibits the lowest activity, as revealed in Fig. 6.

In order to further understand CO oxidation to DMO over Pd<sub>4</sub>Cu<sub>8</sub>/Cu(111) and Pd<sub>1</sub>-Cu(111) at the practical condition with temperatures (T: 375–415 K) and pressures (P<sub>CO</sub>: 280 kPa, P<sub>CH<sub>3</sub>ONO</sub>: 200 kPa) [19], the microkinetic model [11,12,93–96] on the basis of transition state theory is implemented in the present study. Firstly, adsorption equilibrium constants (*K*) of initial reactants (OCH<sub>3</sub> and CO) are acquired by the formulas (5)–(6) when it is assumed that the adsorption processes are in equilibrium. Secondly, the coverage of OCH<sub>3</sub>, CO, COOCH<sub>3</sub> and OCCOOCH<sub>3</sub> are obtained by the formulas (7)–(11). Lastly, the generation rates of DMO and DMC can be obtained the formulas:  $r_{\text{DMO}} = k_3\theta_{\text{COOCH}_3}^2 + k_5\theta_{\text{OCCOOCH}_3}\theta_{\text{OCH}_3}$  (12) and  $r_{\text{DMC}} = k_6\theta_{\text{COOCH}_3}\theta_{\text{OCH}_3}$  (13), respectively. The calculated adsorption equilibrium constants, coverages and formation rates are presented in Table 4,

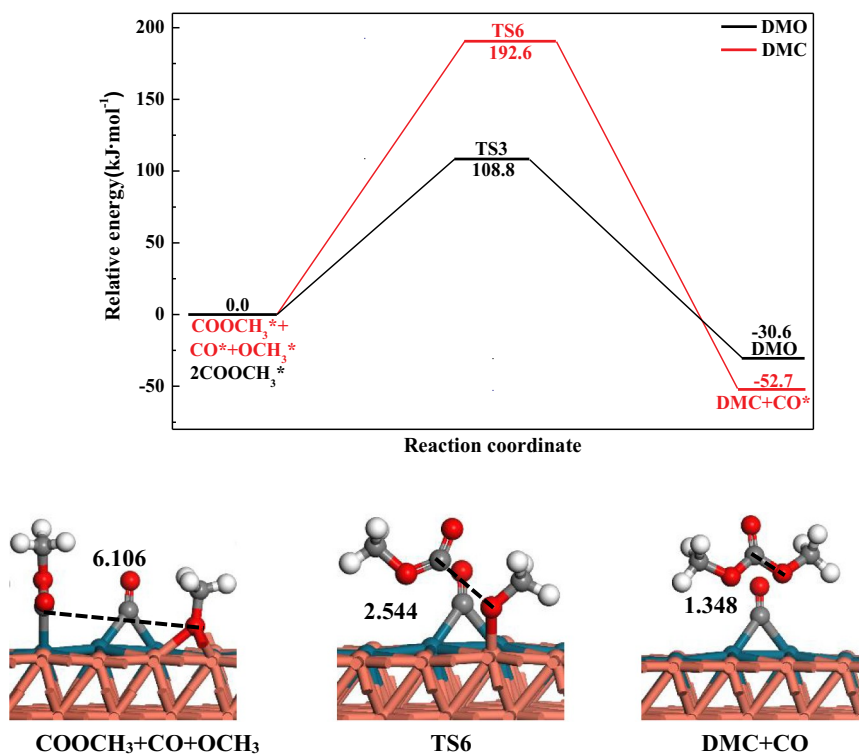


Fig. 4. The comparison of the potential energy profile for the rate-determining step in favorable reaction path toward DMO and DMC synthesis over the Pd<sub>4</sub>Cu<sub>8</sub>/Cu (111) surface.

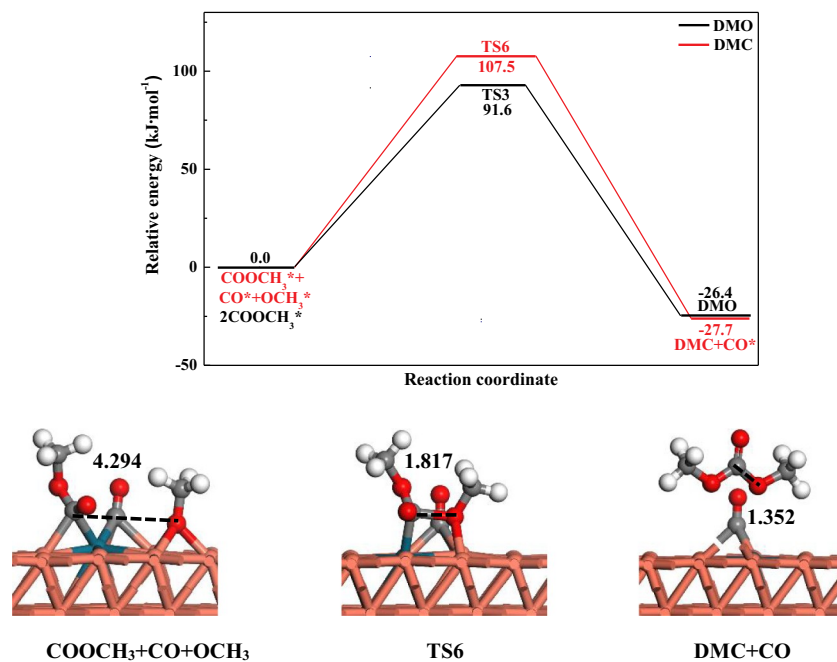


Fig. 5. The comparison of the potential energy profile for the rate-determining step in favorable reaction path toward DMO and DMC synthesis over the Pd<sub>1</sub>-Cu(111) surface.

Table 5, and Table 6, respectively.

$$K = \exp[-(\Delta E_{\text{ads}} - T(S_{\text{adsorbate}} - S_{\text{gas}}))/RT] \tag{5}$$

$$S = R \sum_{i=1}^{3N} \left[ -\ln \left( 1 - \exp \left( -\frac{h\nu_i}{k_B T} \right) \right) + \frac{h\nu_i}{k_B T} \frac{\exp \left( -\frac{h\nu_i}{k_B T} \right)}{1 - \exp \left( -\frac{h\nu_i}{k_B T} \right)} \right] \tag{6}$$

where  $\Delta E_{\text{ads}}$  refers to the adsorption energies of OCH<sub>3</sub> or CO.  $S_{\text{adsorbate}}$  represents entropies of the adsorbed OCH<sub>3</sub> and CO over Pd<sub>4</sub>Cu<sub>8</sub>/Cu(111) and Pd<sub>1</sub>-Cu(111) surfaces.  $S_{\text{gas}}$  represents gas phase entropy, which can be obtained by the Eq. (6) [97].

$$\theta_{\text{CO}} = P_{\text{CO}} K_{\text{CO}} \theta^* \tag{7}$$

$$\theta_{\text{OCH}_3} = P_{\text{OCH}_3} K_{\text{OCH}_3} \theta^* \tag{8}$$

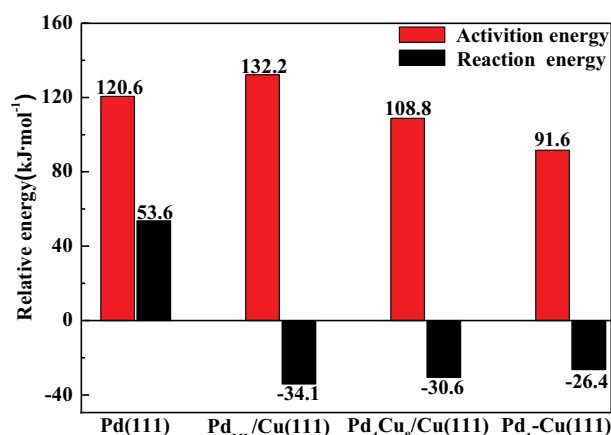


Fig. 6. The reaction energy profile for the speed-determining step ( $2\text{COOCH}_3 \rightarrow \text{DMO}$ ) in optimal path for DMO generation on surfaces of Pd(111), Pd<sub>ML</sub>/Cu(111), Pd<sub>4</sub>Cu<sub>8</sub>/Cu(111) and Pd<sub>1</sub>-Cu(111).

$$\theta_{\text{COOCH}_3} \frac{d\theta_{\text{COOCH}_3}}{dt} = k_1 \theta_{\text{OCH}_3} \theta_{\text{CO}} + k_2 \theta_{\text{OCH}_3} \theta_{\text{CO}} - k_3 \theta_{\text{COOCH}_3}^2 - k_4 \theta_{\text{COOCH}_3} \theta_{\text{CO}} - k_6 \theta_{\text{COOCH}_3} \theta_{\text{OCH}_3} = 0 \quad (9)$$

$$\theta_{\text{OCCOCH}_3} \frac{d\theta_{\text{OCCOCH}_3}}{dt} = k_4 \theta_{\text{COOCH}_3} \theta_{\text{CO}} - k_5 \theta_{\text{OCCOCH}_3} \theta_{\text{OCH}_3} = 0 \quad (10)$$

$$\theta_{\text{CO}} + \theta_{\text{OCH}_3} + \theta_{\text{COOCH}_3} + \theta_{\text{OCCOCH}_3} + \theta^* = 1 \quad (11)$$

As revealed in Table 6, the order of DMO formation rate is Pd<sub>1</sub>-Cu(111) > Pd<sub>4</sub>Cu<sub>8</sub>/Cu(111) > Pd(111) > Pd<sub>ML</sub>/Cu(111) and the rate of DMO generation is found to be far higher than that of DMC formation over Pd<sub>4</sub>Cu<sub>8</sub>/Cu(111) and Pd<sub>1</sub>-Cu(111), which agrees well with the analysis via activation barrier as well as rate constants. As a consequence, Pd<sub>4</sub>Cu<sub>8</sub>/Cu(111) and Pd<sub>1</sub>-Cu(111) surfaces exhibit remarkable activity and selectivity for DMO formation. The same microkinetic analysis has been adopted to acquire that activity for DMO synthesis on the Pd<sub>ML</sub>/Cu(111) was weaker than that on the Pd(111) [12].

### 3.4. Strain versus ligand effect on catalytic activity for DMO synthesis

As mentioned above, the catalytic activity for DMO synthesis is Pd<sub>1</sub>-Cu(111) > Pd<sub>4</sub>Cu<sub>8</sub>/Cu(111) > Pd<sub>ML</sub>/Cu(111), which increases as the amount of Pd decreases. In bimetallic catalysts system, the strain and ligand effect together affect the catalytic activity, where the strain effect occurs when the bond length of surface metal-metal is compressed or expanded by the substrate metal and the ligand effect arises when electrons transfer between two different metal atoms [66–75]. The calculated average bond length between Pd and surrounding atoms on surfaces of Pd(111), Pd<sub>ML</sub>/Cu(111), Pd<sub>4</sub>Cu<sub>8</sub>/Cu(111) and Pd<sub>1</sub>-Cu(111) are 2.797, 2.650 [12], 2.577 and 2.601 Å, respectively, indicating that Cu substrates cause the contraction of average bond length between Pd and surrounding atoms, which is termed the strain effect, as well as the values of contraction strain ( $\xi$ ) are -5.3%, -7.9% and -7.0%, respectively. Average charge polarization ( $\Delta\sigma$ ) of surface Pd atoms over Pd<sub>ML</sub>/Cu(111), Pd<sub>4</sub>Cu<sub>8</sub>/Cu(111) and Pd<sub>1</sub>-Cu(111) are obtained by the Bader charge and the values are -0.14 [12], -0.28, and -0.37 e,

Table 4

The reaction equilibrium constants of CO and OCH<sub>3</sub>.

		375 K	385 K	395 K	405 K	415 K
Pd <sub>4</sub> Cu <sub>8</sub> /Cu(111)	$K_{\text{CO}}$	$2.60 \times 10^7$	$1.25 \times 10^7$	$6.23 \times 10^6$	$3.21 \times 10^6$	$1.71 \times 10^6$
	$K_{\text{OCH}_3}$	$1.48 \times 10^{16}$	$4.63 \times 10^{15}$	$1.53 \times 10^{15}$	$5.36 \times 10^{14}$	$1.97 \times 10^{14}$
Pd <sub>1</sub> -Cu(111)	$K_{\text{CO}}$	$1.65 \times 10^9$	$7.06 \times 10^8$	$3.14 \times 10^8$	$1.46 \times 10^8$	$7.02 \times 10^7$
	$K_{\text{OCH}_3}$	$1.30 \times 10^{14}$	$7.46 \times 10^{13}$	$2.82 \times 10^{13}$	$1.12 \times 10^{13}$	$4.63 \times 10^{12}$

respectively, indicating that the charge transfer to surface Pd from Cu substrates, which is known as the ligand effect. It can be thought that different contents of Pd atoms cause different strain and ligand effects, thereby resulting in different catalytic activity. Nevertheless, the co-existence of the strain and ligand effect conceals underlying origin of the changed activity of bimetallic catalysts. Thence, it is essential to decouple strain and ligand effect so as to comprehend individual impact on activity.

Taking account of calculation efficiency, the speed-controlling step ( $2\text{COOCH}_3 \rightarrow \text{DMO}$ ) that determines the catalytic activity is chosen to investigate how the strain and ligand effect influence the activity of Pd<sub>4</sub>Cu<sub>8</sub>/Cu(111) and Pd<sub>1</sub>-Cu(111). According to previous work [68,71,98], the strain contribution ( $\Delta E_a^{\text{strain}}$ ), the ligand contribution ( $\Delta E_a^{\text{ligand}}$ ) and combined contribution ( $\Delta E_a^{\text{combined}}$ ) can be calculated via Eqs. (14)–(16), where  $E_a^{\text{Strain-M}}$  stands for the activation barrier on strained monometallic Pd(111) surface,  $E_a^{\text{Pd}}$  refers to the activation barrier on the Pd(111) surface,  $E_a^{\text{Pd-M}}$  represents the activation barrier on Pd<sub>4</sub>Cu<sub>8</sub>/Cu(111) or Pd<sub>1</sub>-Cu(111) surfaces. For instance, on the Pd<sub>4</sub>Cu<sub>8</sub>/Cu(111), based on the calculated  $E_a^{\text{Strain-M}}$ ,  $E_a^{\text{Pd}}$  and  $E_a^{\text{Pd-M}}$  (172.5, 120.6 and 108.8 kJ/mol) combined with Eqs. (14)–(16),  $\Delta E_a^{\text{strain}}$ ,  $\Delta E_a^{\text{ligand}}$  and  $\Delta E_a^{\text{combined}}$  can be obtained and the values are 51.9, -63.7 and -11.8 kJ/mol, respectively.

$$\Delta E_a^{\text{strain}} = E_a^{\text{Strain-M}} - E_a^{\text{Pd}} \quad (14)$$

$$\Delta E_a^{\text{ligand}} = E_a^{\text{Pd-M}} - E_a^{\text{Strain-M}} \quad (15)$$

$$\Delta E_a^{\text{combined}} = \Delta E_a^{\text{strain}} + \Delta E_a^{\text{ligand}} \quad (16)$$

In the case of Pd<sub>4</sub>Cu<sub>8</sub>/Cu(111) surface, the strain effect enlarges the activation energy while ligand effect is opposite, where the ligand effect is dominant factor, therefore its catalytic is enhanced, as revealed in Fig. 7. On the surface of Pd<sub>1</sub>-Cu(111), strain effect has a decrease on activation barrier while ligand effect has an increase on it, and strain effect prevails to ligand effect, leading to the catalytic activity increased, which is similar to the case over Pd<sub>ML</sub>/Co(111) and Pd<sub>ML</sub>/Ni(111) [11]. This method has been also successfully employed in explaining that the relatively low activity for DMO generation on the Pd<sub>ML</sub>/Cu(111) was because weak strain effect reduced activation barrier while strong ligand effect enlarged it [12].

## 4. Conclusions

Density functional theory (DFT) and microkinetic model have been employed in studying CO oxidation to DMO over Pd<sub>4</sub>Cu<sub>8</sub>/Cu(111) and Pd<sub>1</sub>-Cu(111) surfaces to search low Pd usage of Pd–Cu bimetallic catalysts in the presupposition of keeping its catalytic performance. It has been obtained that the optimal pathway is  $\text{CO} + \text{CH}_3\text{O} \rightarrow \text{COOCH}_3 + (\text{CO} + \text{OCH}_3) \rightarrow 2\text{COOCH}_3 \rightarrow \text{DMO}$  over these two catalysts, in which the rate-determining step is  $2\text{COOCH}_3 \rightarrow \text{DMO}$ . The analysis result of energy barrier in conjunction with microkinetic model indicates that the activity for DMO formation is in sequence of Pd<sub>1</sub>-Cu(111) > Pd<sub>4</sub>Cu<sub>8</sub>/Cu(111) > Pd(111) > Pd<sub>ML</sub>/Cu(111). The outstanding activity of Pd<sub>4</sub>Cu<sub>8</sub>/Cu(111) for DMO formation are ascribed to weak strain effect and strong ligand effect, where strain effect increases activation barrier while ligand effect reduces it. The opposite of this arises over the Pd<sub>1</sub>-Cu(111) surface. In addition, DMO formation is favorable than synthesis of side-product (DMC) on surfaces of Pd<sub>4</sub>Cu<sub>8</sub>/



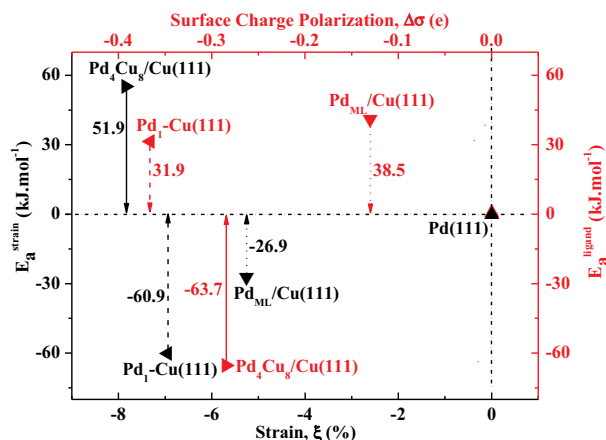
**Table 5**  
The surface coverage for different species.

		375 K	385 K	395 K	405 K	415 K
Pd <sub>4</sub> Cu <sub>8</sub> /Cu(111)	$\theta^*$	$1.69 \times 10^{-23}$	$6.16 \times 10^{-23}$	$2.10 \times 10^{-22}$	$6.71 \times 10^{-22}$	$2.03 \times 10^{-21}$
	$\theta_{CO}$	$1.23 \times 10^{-10}$	$2.15 \times 10^{-10}$	$3.65 \times 10^{-10}$	$6.04 \times 10^{-10}$	$9.73 \times 10^{-10}$
	$\theta_{OCH_3}$	$5.01 \times 10^{-2}$	$5.70 \times 10^{-2}$	$6.43 \times 10^{-2}$	$7.20 \times 10^{-2}$	$8.01 \times 10^{-2}$
	$\theta_{COOCH_3}$	$9.50 \times 10^{-1}$	$9.43 \times 10^{-1}$	$9.36 \times 10^{-1}$	$9.28 \times 10^{-1}$	$9.20 \times 10^{-1}$
	$\theta_{OCCOCH_3}$	$4.31 \times 10^{-23}$	$1.60 \times 10^{-22}$	$5.57 \times 10^{-22}$	$1.82 \times 10^{-21}$	$5.62 \times 10^{-21}$
Pd <sub>1</sub> -Cu(111)	$\theta^*$	$2.81 \times 10^{-20}$	$5.28 \times 10^{-20}$	$1.42 \times 10^{-19}$	$3.62 \times 10^{-19}$	$8.83 \times 10^{-19}$
	$\theta_{CO}$	$1.30 \times 10^{-5}$	$1.04 \times 10^{-5}$	$1.25 \times 10^{-5}$	$1.48 \times 10^{-5}$	$1.74 \times 10^{-5}$
	$\theta_{OCH_3}$	$7.33 \times 10^{-1}$	$7.88 \times 10^{-1}$	$7.99 \times 10^{-1}$	$8.09 \times 10^{-1}$	$8.18 \times 10^{-1}$
	$\theta_{COOCH_3}$	$2.67 \times 10^{-1}$	$2.12 \times 10^{-1}$	$2.01 \times 10^{-1}$	$1.91 \times 10^{-1}$	$1.82 \times 10^{-1}$
	$\theta_{OCCOCH_3}$	$3.27 \times 10^{-14}$	$3.54 \times 10^{-14}$	$7.03 \times 10^{-14}$	$1.35 \times 10^{-13}$	$2.50 \times 10^{-13}$

**Table 6**  
The generation rates ( $s^{-1}\text{site}^{-1}$ ) for DMO and DMC.

		375 K	385 K	395 K	405 K	415 K
Pd <sub>4</sub> Cu <sub>8</sub> /Cu(111)	DMO	$4.07 \times 10^{-3}$	$1.00 \times 10^{-2}$	$2.36 \times 10^{-2}$	$5.33 \times 10^{-2}$	$1.15 \times 10^{-1}$
	DMC	$9.43 \times 10^{-16}$	$5.46 \times 10^{-15}$	$2.88 \times 10^{-14}$	$1.40 \times 10^{-13}$	$6.30 \times 10^{-13}$
Pd <sub>1</sub> -Cu(111)	DMO	$6.88 \times 10^{-1}$	$9.47 \times 10^{-1}$	$1.79 \times 10^0$	$3.27 \times 10^0$	$5.81 \times 10^0$
	DMC	$1.87 \times 10^{-4}$	$3.90 \times 10^{-4}$	$8.76 \times 10^{-4}$	$1.89 \times 10^{-3}$	$3.91 \times 10^{-3}$
Pd(111) <sup>a</sup>	DMO	$4.72 \times 10^{-6}$	$1.29 \times 10^{-5}$	$3.35 \times 10^{-5}$	$5.31 \times 10^{-5}$	$1.98 \times 10^{-4}$
	DMC	$4.02 \times 10^{-14}$	$2.45 \times 10^{-13}$	$1.11 \times 10^{-12}$	$4.02 \times 10^{-12}$	$6.04 \times 10^{-12}$
Pd <sub>ML</sub> /Cu(111) <sup>a</sup>	DMO	$7.92 \times 10^{-7}$	$2.42 \times 10^{-6}$	$6.98 \times 10^{-6}$	$1.91 \times 10^{-5}$	$2.71 \times 10^{-5}$
	DMC	$5.67 \times 10^{-20}$	$4.44 \times 10^{-19}$	$3.14 \times 10^{-18}$	$2.01 \times 10^{-17}$	$2.96 \times 10^{-17}$

<sup>a</sup> The study in Ref [12].



**Fig. 7.** The comparison of strain contribution and ligand contribution for  $2COOCH_3 \rightarrow DMO$ .

Cu(111) and Pd<sub>1</sub>-Cu(111). Hence, we suggest that the Pd<sub>4</sub>Cu<sub>8</sub>/Cu(111) and Pd<sub>1</sub>-Cu(111) can be attempted in experiment to improve the performance of catalytic DMO formation and cut down the cost.

## Acknowledgments

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